

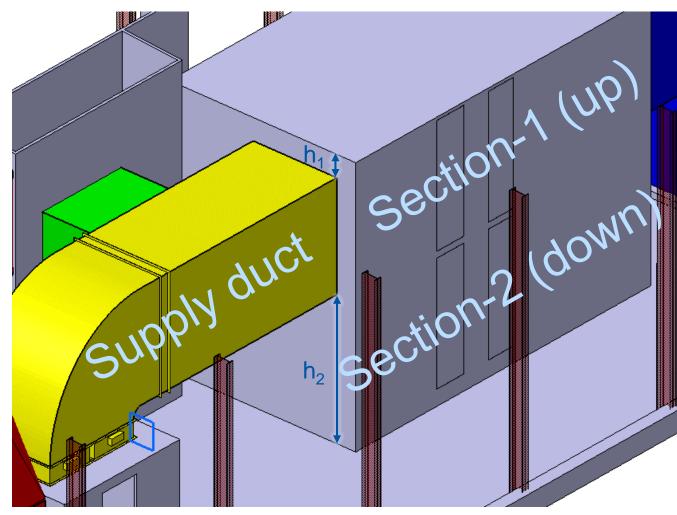
# Some CFD simulations for a 2 stream Air Handler Unit



10/13/2015

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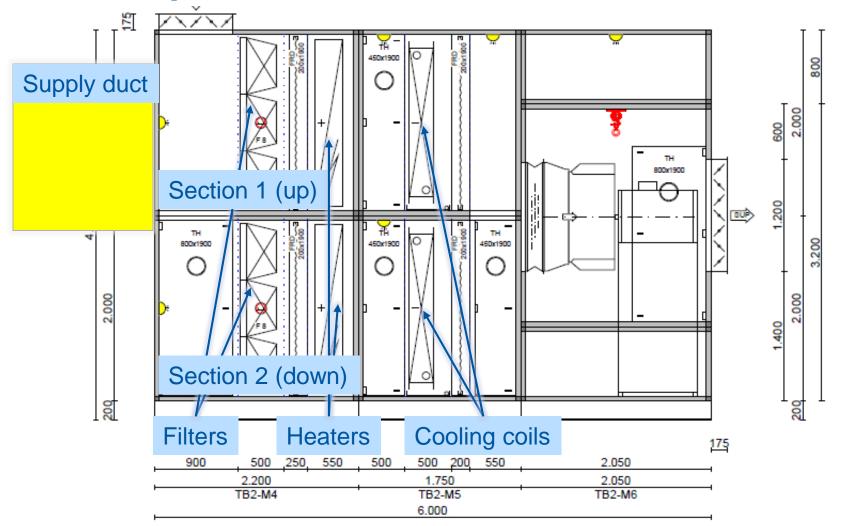
# 2 stream AHU geometry



Problem: will the high positioning of supply air duct (see  $h_1 < h_2$ ) result in uneven flow rate distribution of the two sections?

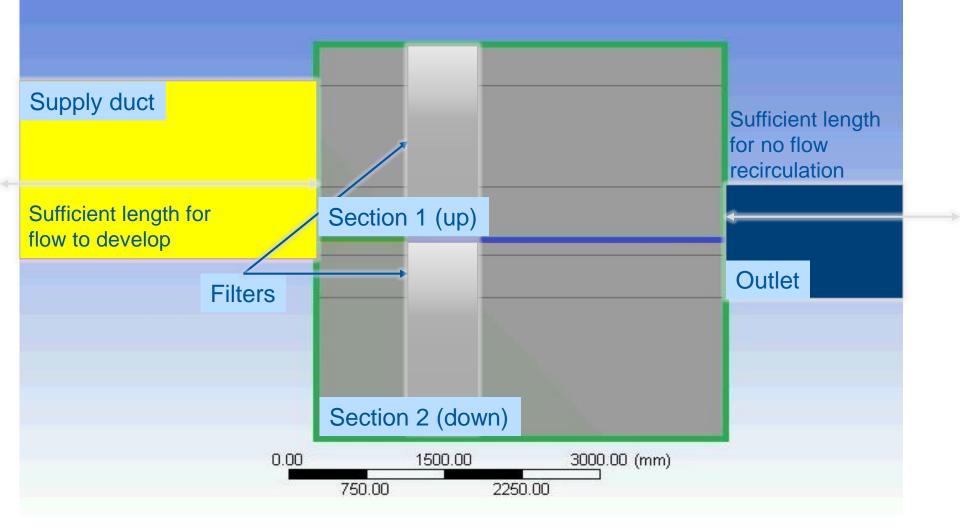


### **2D** representation





# Numerical model (not to scale)





# Numerical model

#### Fluid properties:

Density (ρ)	1.225	kg/m <sup>3</sup>
Dynamic viscosity (v)	1.79*10 <sup>-5</sup>	Pas

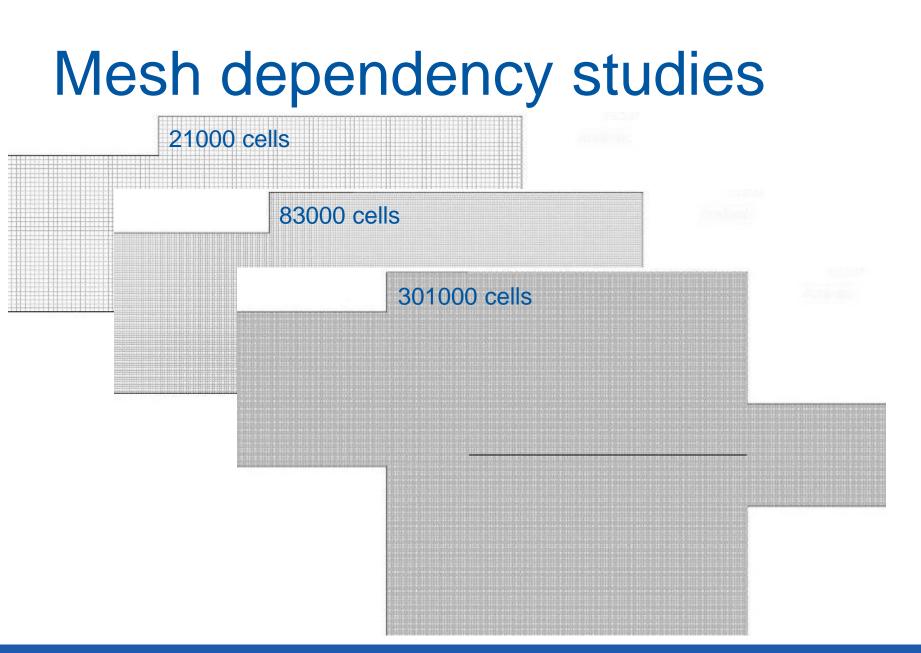
#### Supply properties for the 2D model:

Duct height	1.7 m	Inlet cross section	1.7 m <sup>2</sup>
2D section considered	1 m	Hydraulic diameter	1.26

#### Flow properties:

Volume flow rate	70000 m³/h
Inlet mean velocity	11.4 m/s







### Parametrisation of porous zone

- Pressure loss due to the filter added as a source in the momentum equation
- Parameterised as an inertial loss term in the flow direction

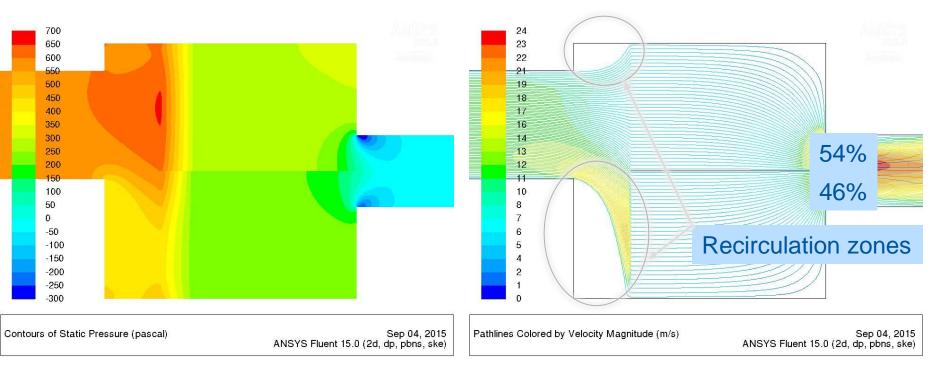
$$\Delta p = C * l * \frac{\rho}{2} v^2$$

Where p is pressure, C [1/m] is viscous resistance, I is the length of the filter,  $\rho$  is density and v assuming flow in the whole cross section.

 In the transversal direction a considerably larger value is given to discourage flow in that direction.



### Base geometry with filter modelled



#### Pressure builds up before the filter which helps to even out the flow.

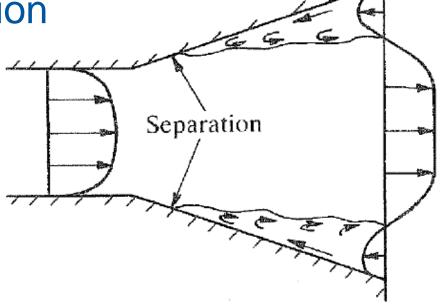
Note the increase in the pressure scale due to the pressure loss in the filter



# Option of adding a diffuser

- Decreases velocity, increases pressure
- Care must be taken with the angle
- Separation increases pressure loss and unevens flow distribution

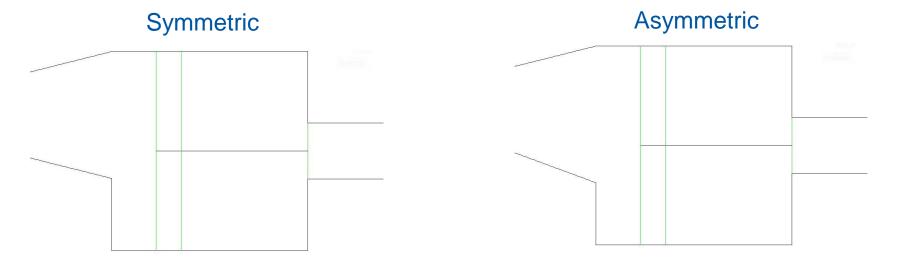
From Miller – Internal Flow Systems





# Tested diffuser geometries I

Diffuser length 1.7 m



Top and bottom chamfered by 0.425 m

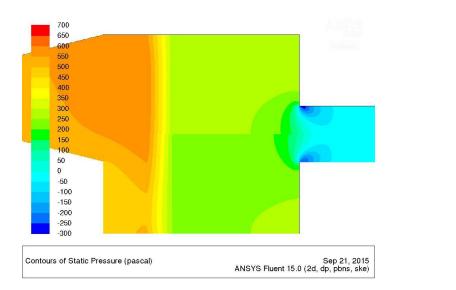
Top chamfered by 0.425 m, bottom by 0.625 m

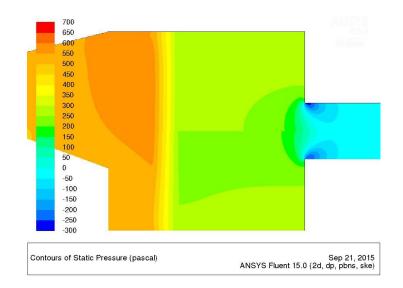


# **Pressure build-up**

#### Symmetric







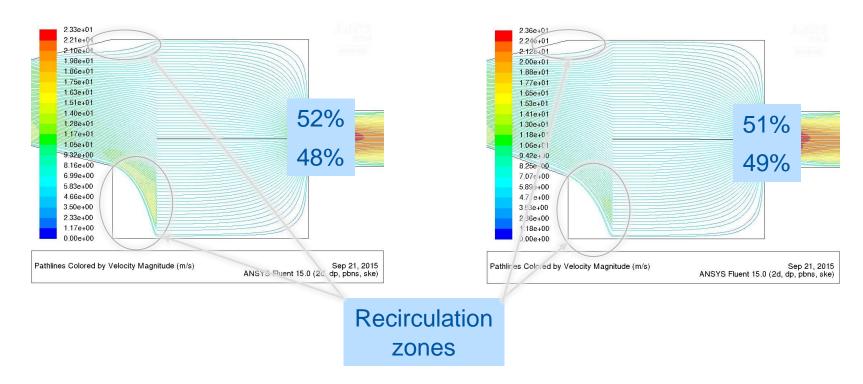
Due to the less abrupt change in pressure compared to the sudden opening version, and to the smaller recirculation zones (see next slide): overall pressure loss in the system is reduced by ~62Pa ~77Pa



### Streamline structure and flow rates

#### Symmetric

#### Asymmetric



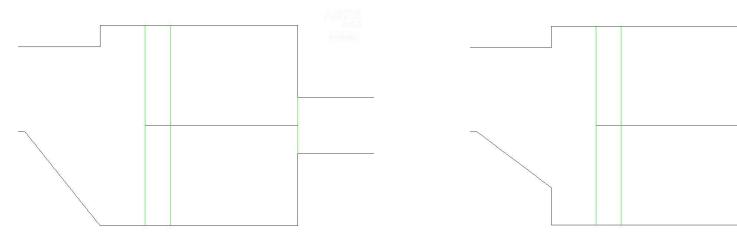


# Tested diffuser geometries II

Diffuser length 1.5 m

Asymmetric 2

Asymmetric 3



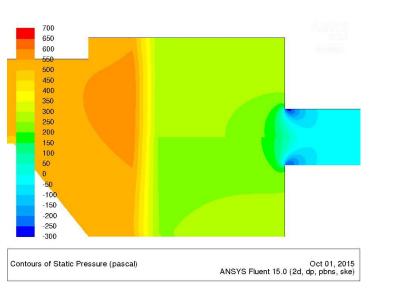
Bottom chamfered till edge

Bottom chamfered by 0.925 m

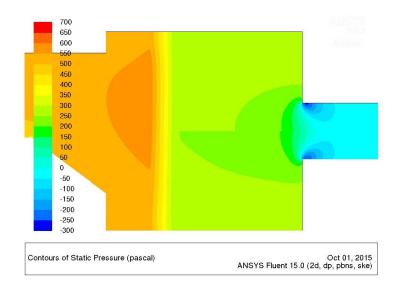


### **Pressure build-up**

#### Asymmetric 2



#### Asymmetric 3



#### Overall pressure loss in the system is reduced by ~71Pa

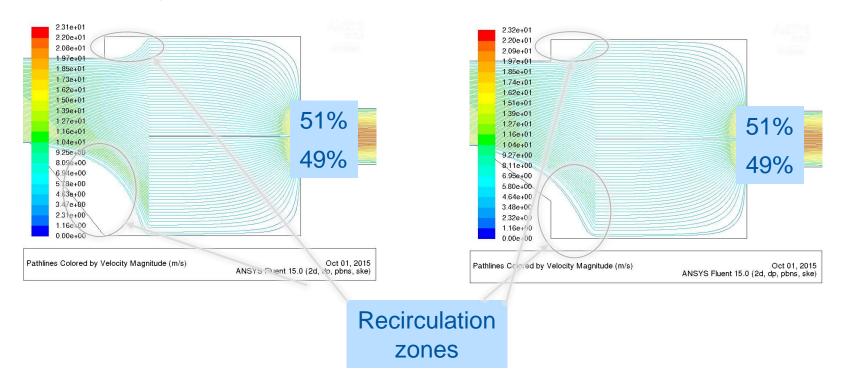
80~Pa



### Streamline structure and flow rates

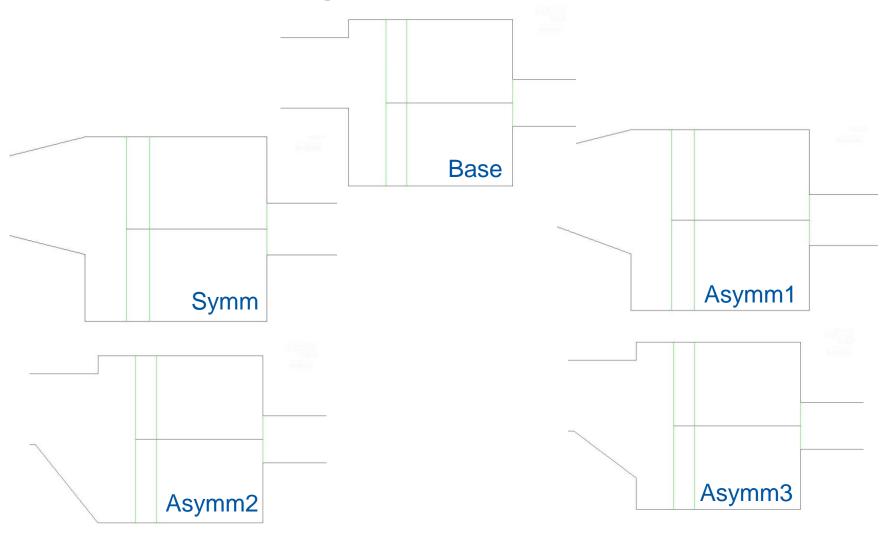
#### Asymmetric 2

#### Asymmetric 3



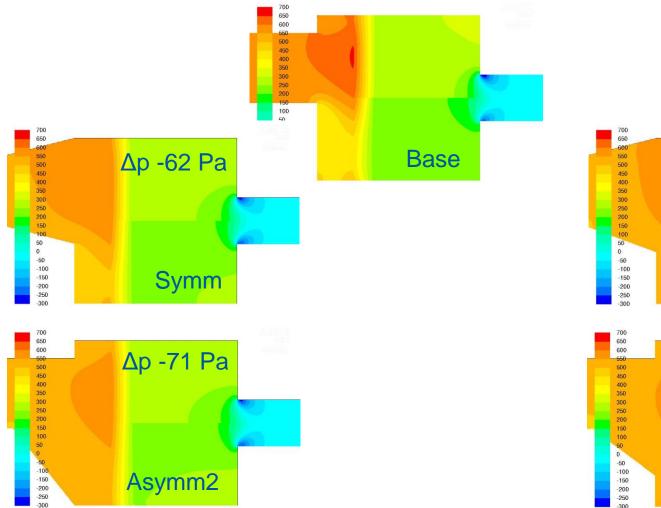


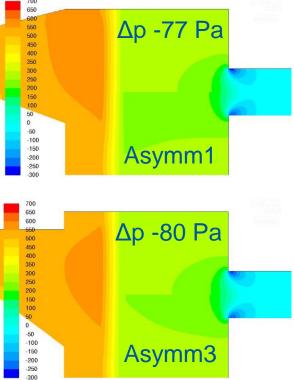
### All tested geometries





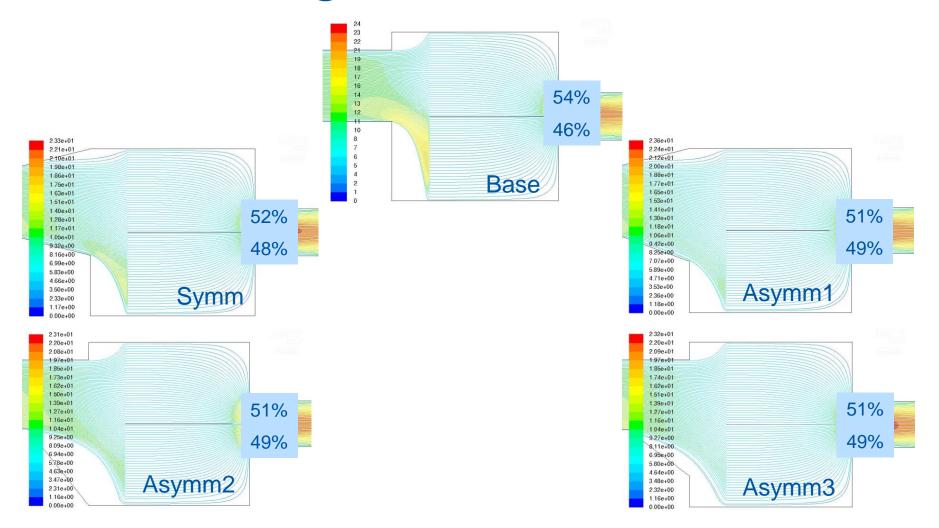
### All tested geometries







### All tested geometries





# Conclusions

- The 2D calculations show 54-46% flow rate inequality for the base setup with only the filter modelled;
- This can be improved by the installation of a diffuser-like gain geometry;
- The diffuser can also cause pressure loss reduction in the system.

	Diffuser geometry variations				
	Symm	Asymm1	Asymm2	Asymm3	
Pressure loss reduction	62 Pa	77 Pa	71 Pa	80 Pa	
Flow rate ratio	52%-48%	51%-49%	51%-49%	<b>51%-49%</b>	



# Thank you for your attention!



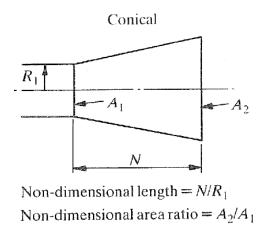
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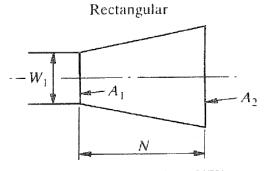
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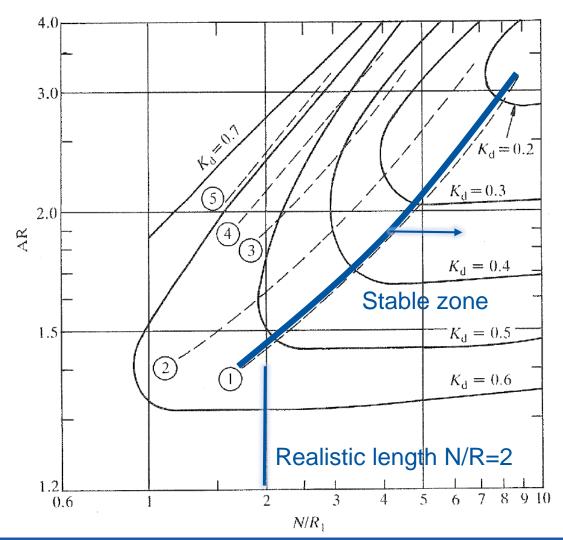
www.cern.ch

### Flow stability in a diffuser - theory





Non-dimensional length =  $N/W_1$ Non-dimensional area ratio =  $A_2/A_1$ 





# Results with empty sections

