

# Summary: thermal analysis, CFD simulations

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**Workshop on SiPM cooling for Fiber Tracker, 17 October 2013**

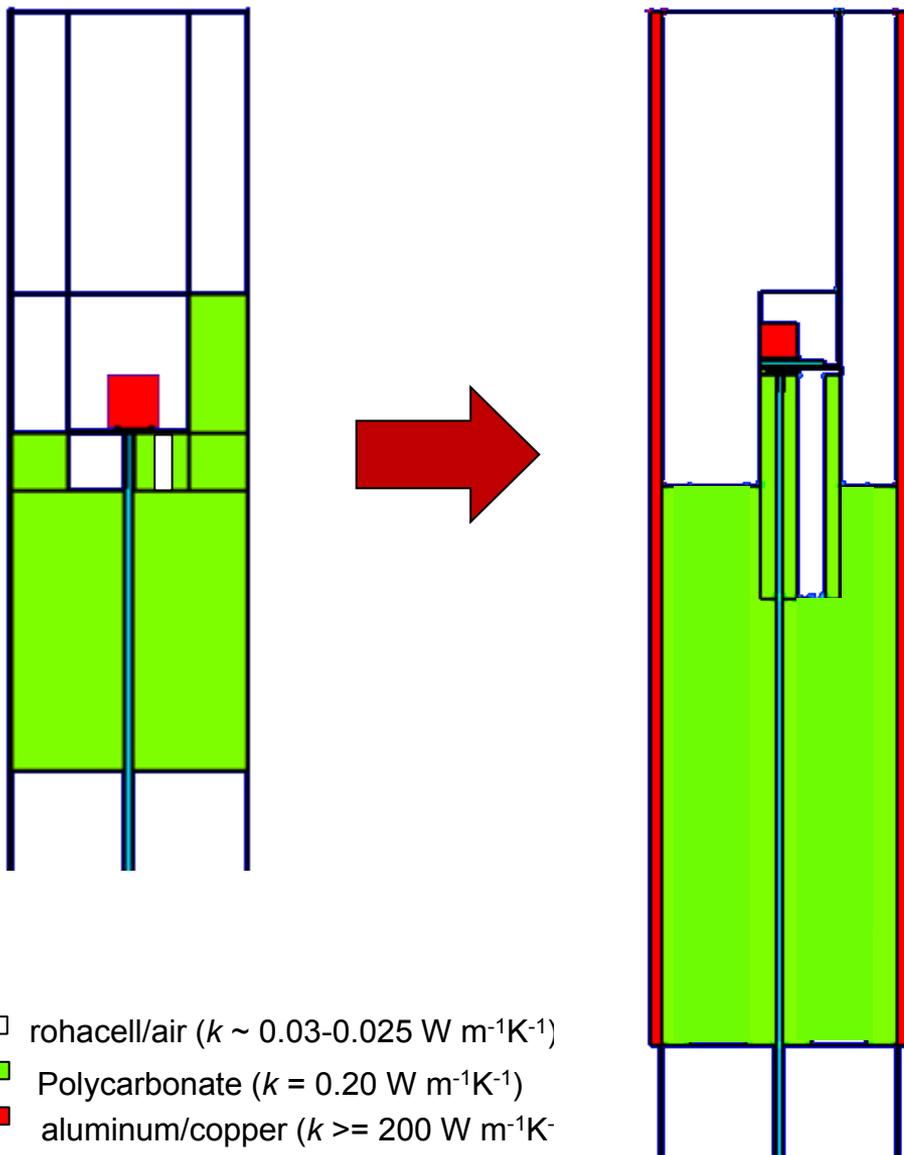


# Contents

- A. Computational Fluid Dynamics (CFD) simulations for design optimization and heat load estimation
  
- B. Comparison among different cooling options (air cooling, liquid cooling, two-phase cooling)

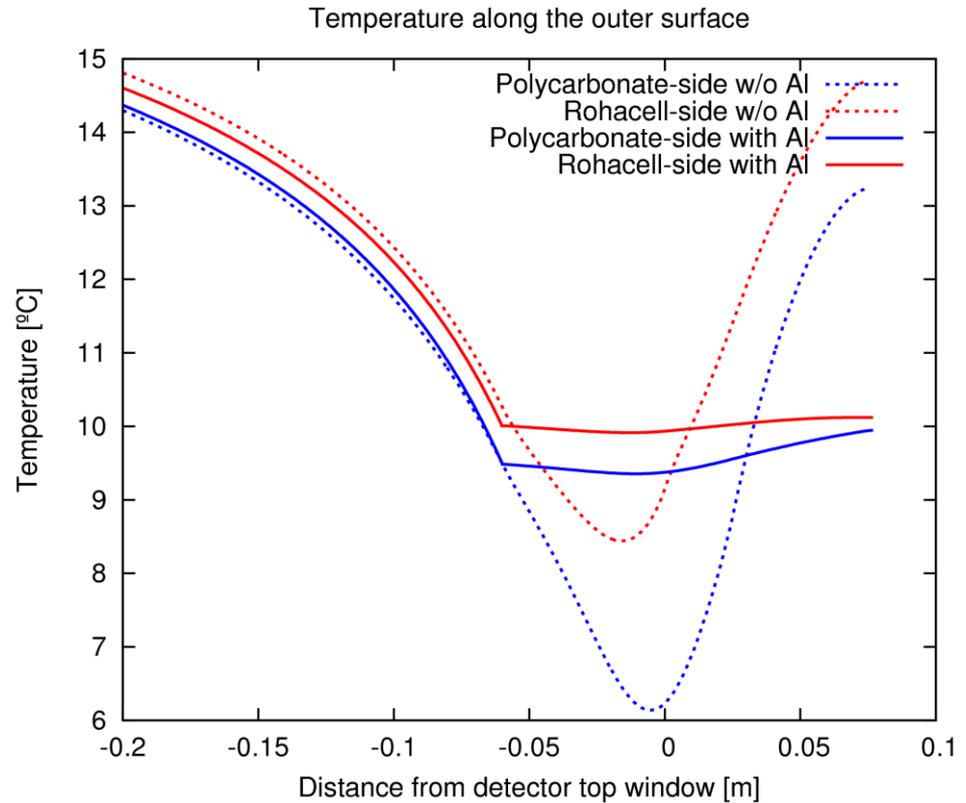
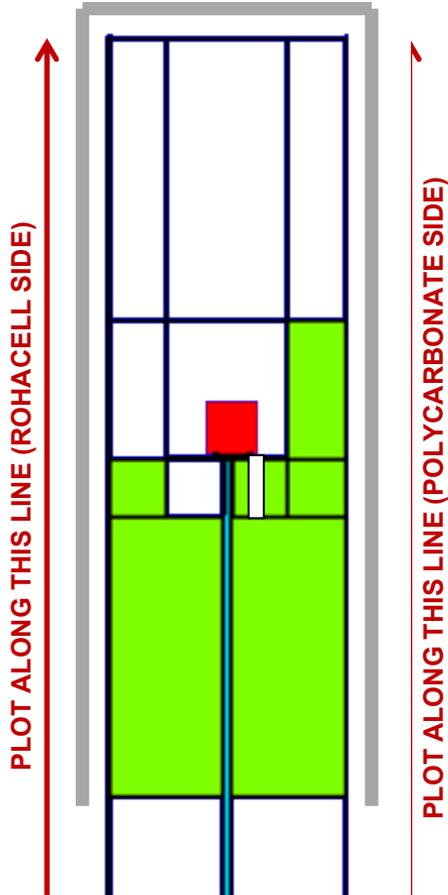
## CFD simulations

- 2D and 3D Computational Fluid Dynamics simulations were run to support the design optimization and identify bottlenecks.
- Direct simulation of natural convection of air around the module and heat conduction inside the modules.
  
- Main parameters to check:
  1. Total module heat load;
  2. Module surface temperature (avoid vapor condensation);
  3. Scintillating fiber temperature (should be as uniform as possible);
  4. Refrigerant to silicon-die temperature difference.

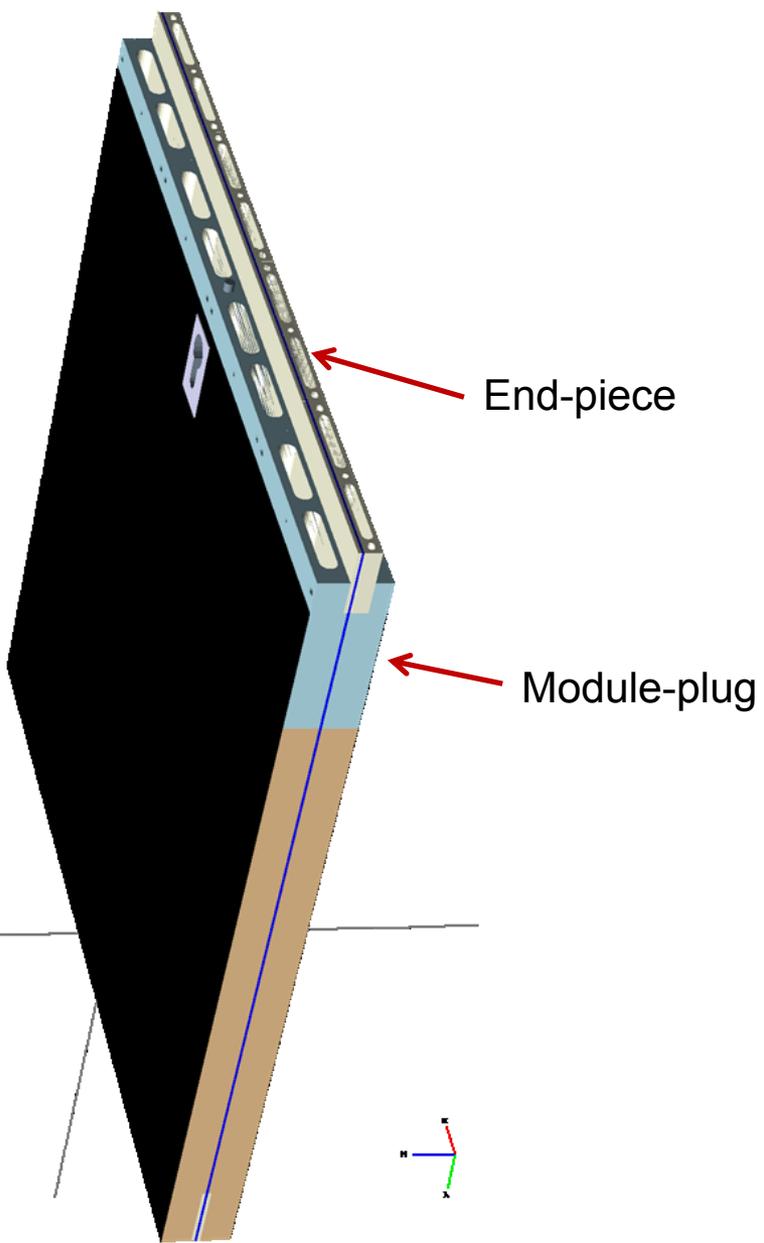


Major optimization steps/issues:

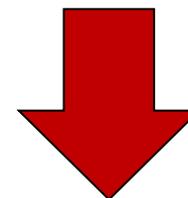
1. Carbon fiber -> kapton;
2. Polycarbonate -> rohacell;
3. Aluminum skin;
4. Grooves to reduce conduction through polycarbonate;
5. Stiffener material choice;
6. Gap fill between modules.



- 2 mm thick aluminum skin covering the module down to the polycarbonate “module plug” (see sketch).
- Temperature in the cold-spot on polycarbonate side is increased by more than 3 K.

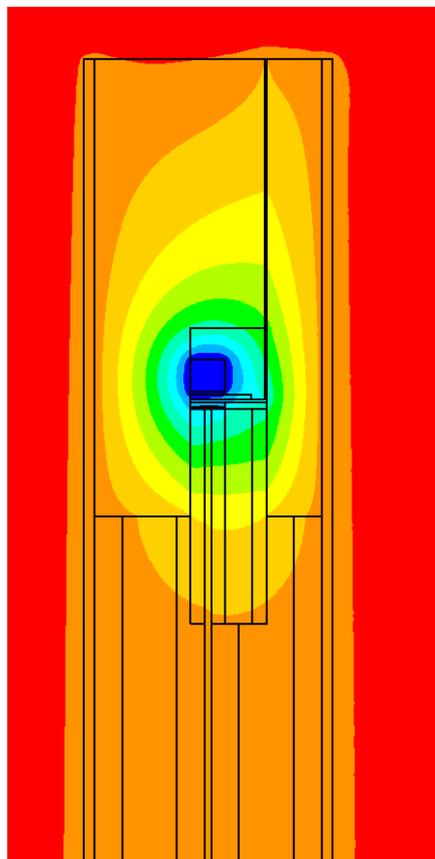


- Polycarbonate display a thermal conductivity  $\sim 10x$  air conductivity.



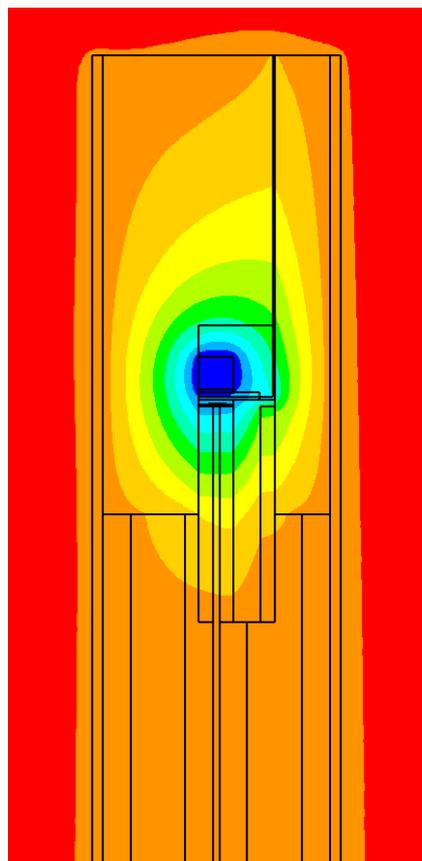
- Grooves can be made in the polycarbonate pieces (module-plug and end-piece) to reduce the heat load.

WITHOUT GROOVES

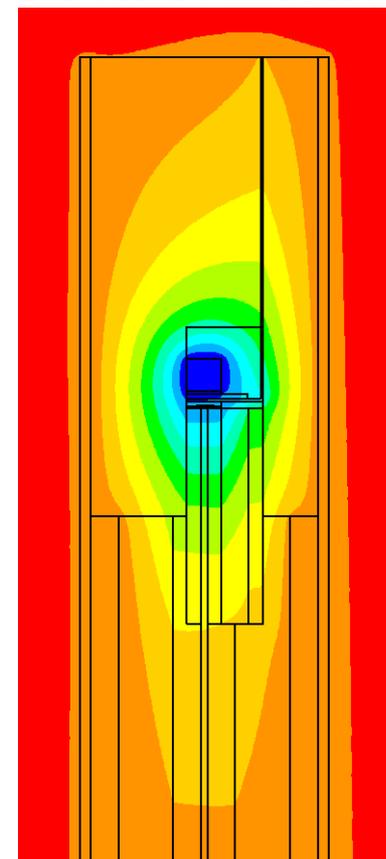


~7.3 W per module

GROOVES IN END-PIECE ONLY



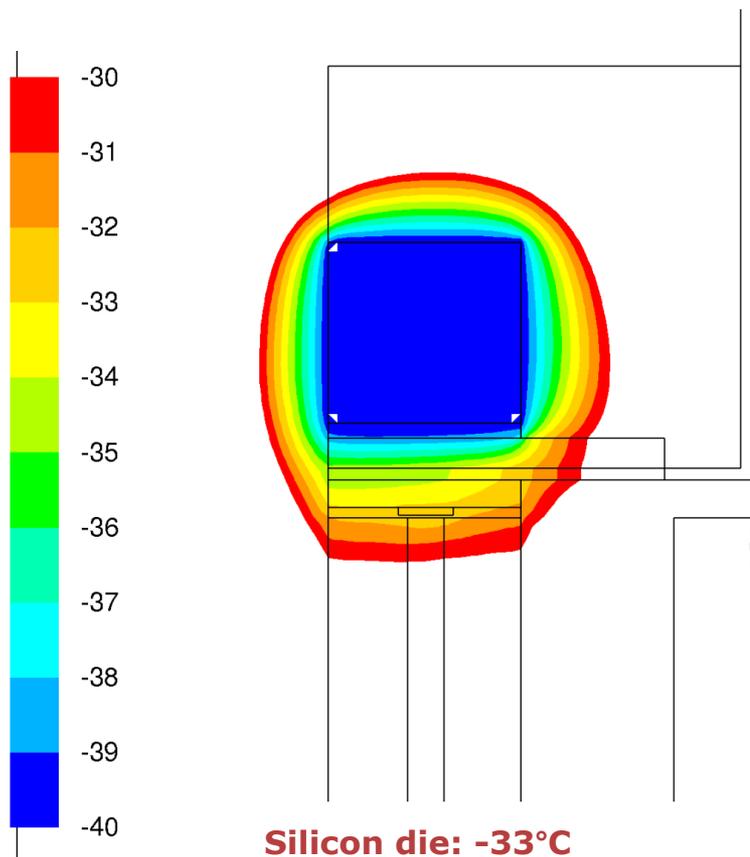
~6.2 W per module

WITH GROOVES IN  
END-PIECE + MODULE PLUG

~5.7 W per module

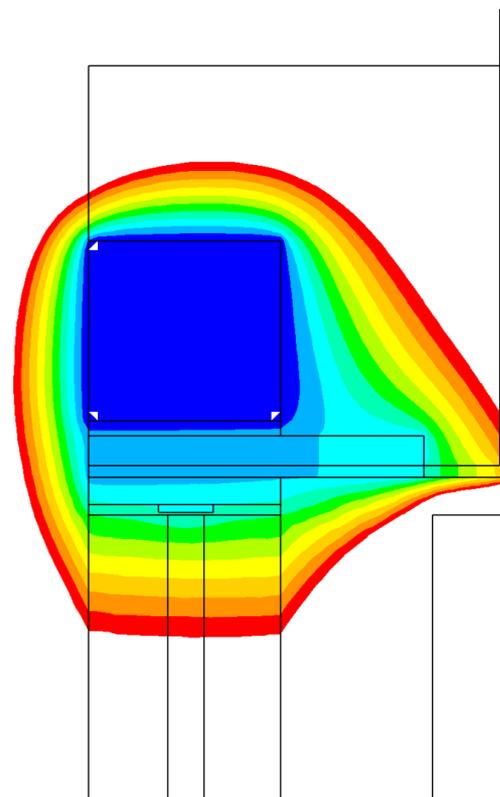
- Grooves in polycarbonate reduces the total heat load;
- On the other hand, grooves in the module-plug reduces the temperature of the scintillating fibers over the last 0.1 m;

$k = 0.25 \text{ W m}^{-1}\text{K}^{-1}$  STIFFENER (FR-4)



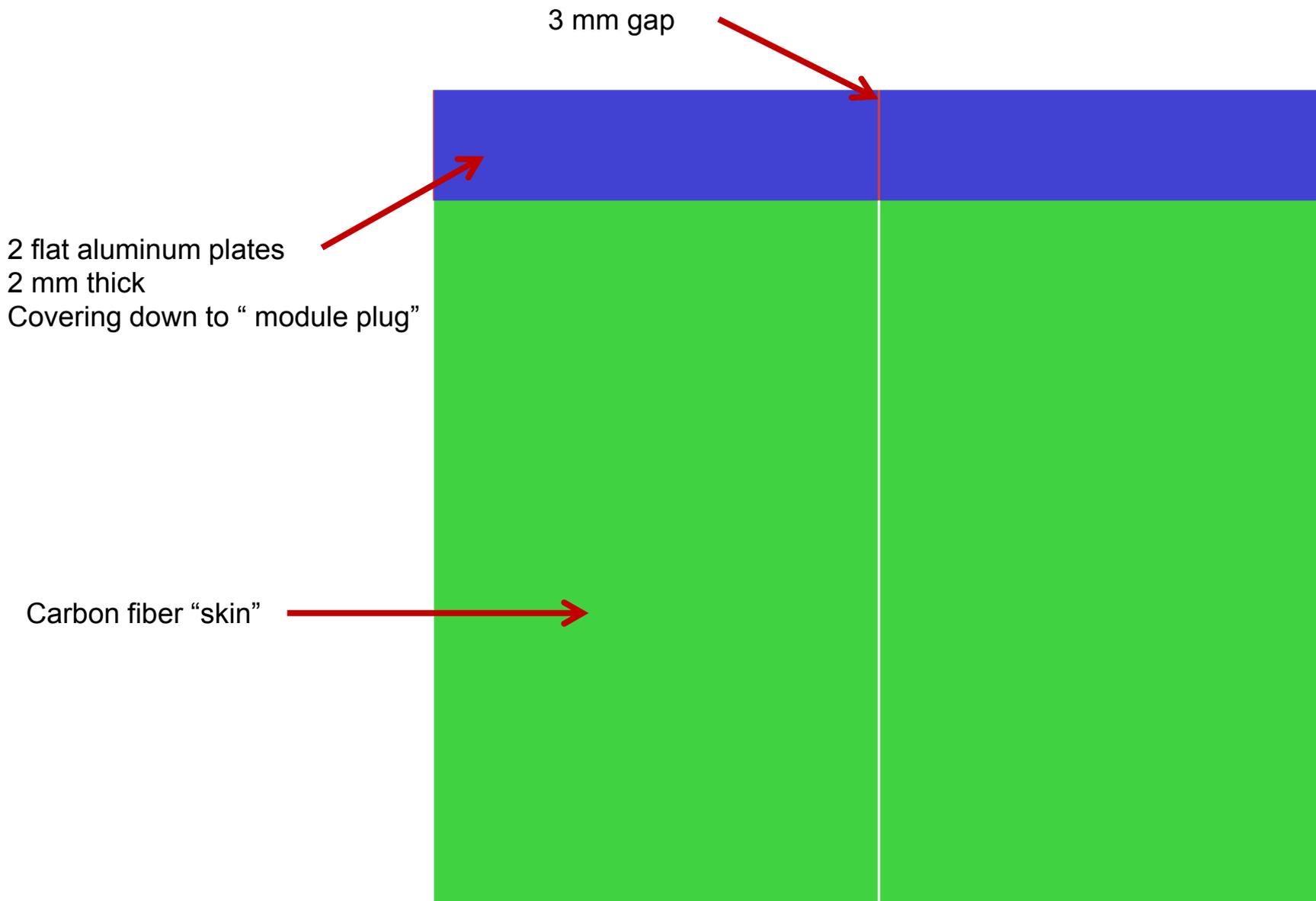
**Silicon die: -33°C**  
**~5.7 W per module**

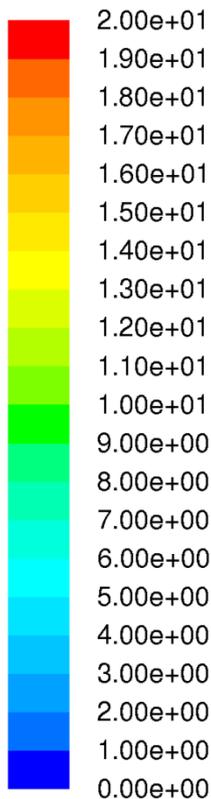
$k = 37 \text{ W m}^{-1}\text{K}^{-1}$  STIFFENER (CERAMIC)



**Silicon die: -37°C**  
**~6.3 W per module**  
**(more heat through flex-cable)**

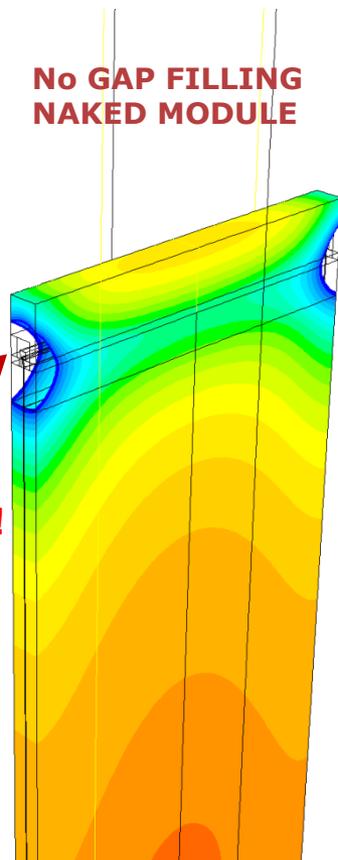
- Despite the heat load increase, high-conductivity stiffener is to be preferred to reduce the refrigerant-to-silicon-die temperature difference (higher refrigerant temperature required).





**VERY COLD SPOT!**

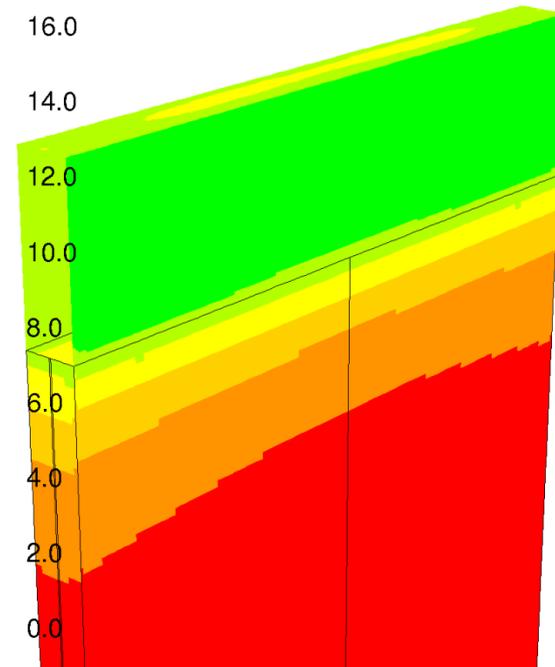
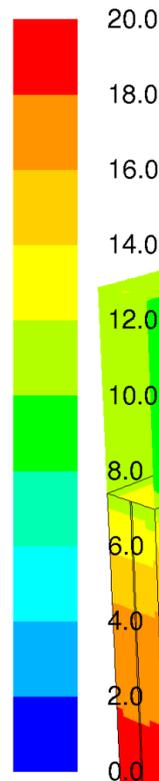
**No GAP FILLING  
NAKED MODULE**



Contours of Static Temperature (c)

**2 mm ALUMINUM PLATES + CF SKIN +  
3mm GAP FILLED WITH  $k=0.1 \text{ Wm}^{-1}\text{K}^{-1}$  MATERIAL**

**~7.1 W per module**



Contours of Static Temperature (c)

- Gap between modules must absolutely be filled with some material, in order to avoid condensation and even frost formation;
- Suggested design: 3 mm gap filled + aluminum plates covering down to module plug + carbon fiber skin on the rest of the module.

# A. CONCLUSIONS

- **Total heat load is expected to be O(10 W);**
- Water vapor condensation is expected not to be a major problem for the present module design;
- Grooves are suggested only in the polycarbonate end-piece;
- Aluminum plates covering the module-plug are suggested to 'flatten' the surface temperature distribution and avoid condensation;
- The 3 mm gap between module must be filled;
- High thermal conductivity stiffener is to be preferred to reduce the refrigerant-to-silicon-die temperature difference.

## **B. Comparison among different cooling options:**

- ) air cooling**
- ) liquid cooling**
- ) two-phase cooling**

## 1. Refrigerant temperature rise ( $\Delta T_{\text{out-in}}$ ):

- It must be low enough to achieve the desired temperature uniformity along the silicon die (< **10 K**);
- For “air-cooling” and “liquid-cooling” it depends on:
  - ) mass flow rate [kg/s];
  - ) specific heat [J/(kg K)].
- During “two-phase” boiling there is no temperature rise, just some temperature drop due to the pressure drop (usually negligible);
- “Two-phase” better than “liquid-cooling” better than “air-cooling”.

## 2. Temperature difference between wall and refrigerant ( $\Delta T_{\text{wall-ref}}$ ):

- Must be low in order to keep the refrigerant temperature reasonably close to  $-40^{\circ}\text{C}$  (i.e.  $>-50^{\circ}\text{C}$ );
- It depends on:
  - ) Heat Transfer Coefficient (HTC) [W/(m<sup>2</sup>K)];
  - ) Surface [m<sup>2</sup>] available for heat transfer;
- The HTC heavily depends on thermodynamic properties and turbulence;
- “Two-phase” better than “liquid-cooling” better than “air-cooling”.

## 3. Pressure drop:

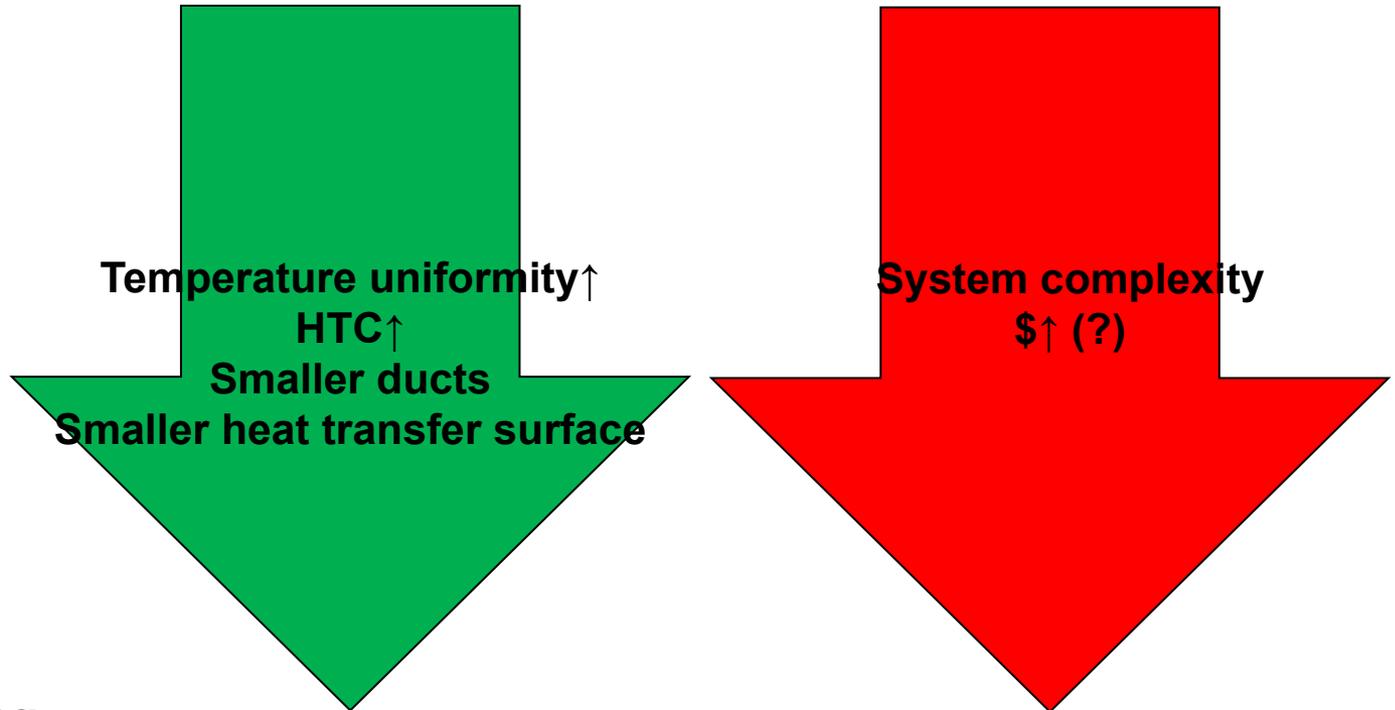
- It must be reasonably low.

Generally speaking:

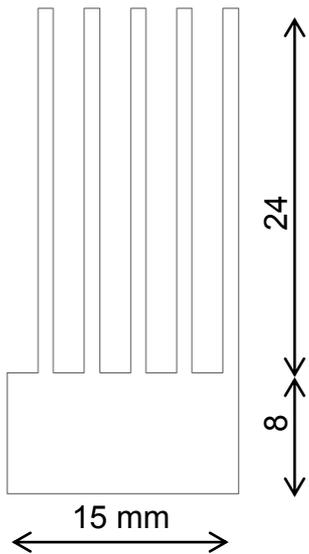
**Air-cooling**

**Liquid-cooling**

**Two-phase cooling**

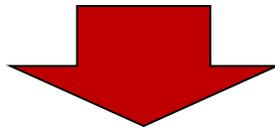


Pitch: 3 mm  
 Fin thickness: 1 mm



- Compressed air and vortex tube to produce cold air (-50°C);
- Heat-sink can be closed to create channels, air leaks could anyhow be beneficial to keep the enclosure in overpressure;
- Estimation based on 10 W assumption:

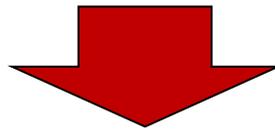
Refrigerant	$\Delta T_{\text{out-in}}$ [K]	HTC [W m <sup>-2</sup> K <sup>-1</sup> ]	$\Delta T_{\text{wall-ref}}$ [K]	$\Delta p$ [Pa]	Flow Rate [NI min <sup>-1</sup> ]
Air (-50°C)	<b>10.6</b>	26	<b>3.0</b>	63	48



- Due to the low temperature uniformity and low power density required, air cooling would provide acceptable temperature uniformity, HTC and pressure drop;

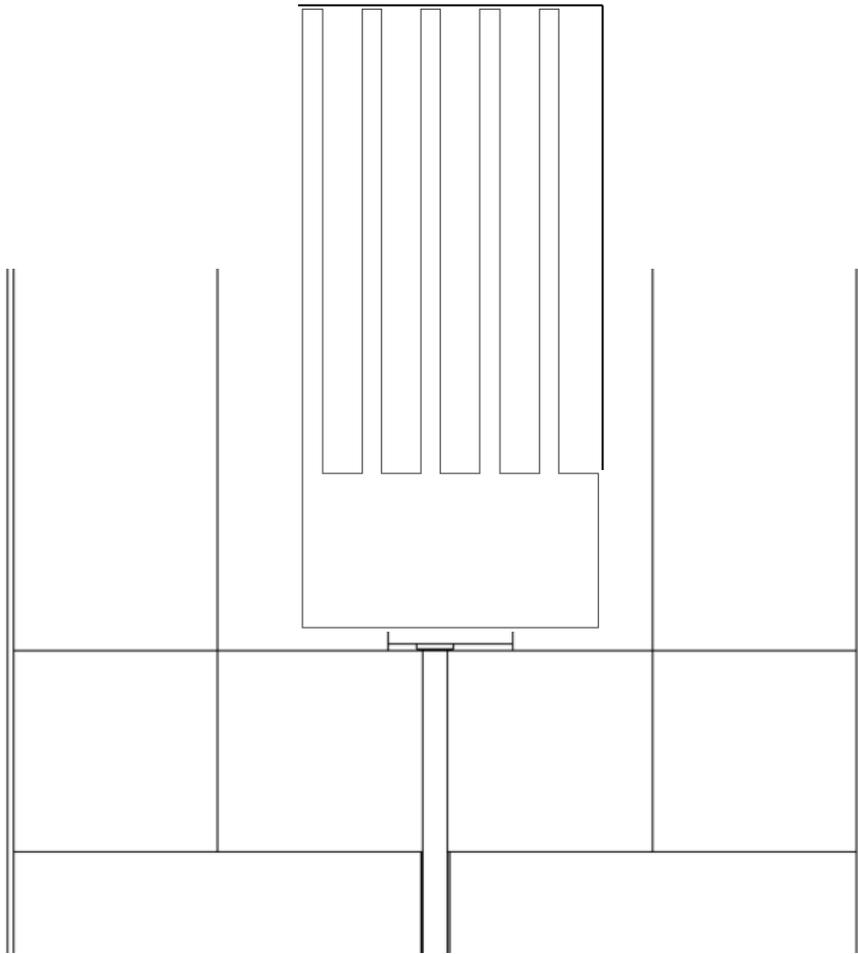
### BUT

- Compressed air needed @ room temperature is around 8x times the cold air produced @ -40°C;
- Air must be dry (dew point -70°C!) to avoid ice formation in the vortex tube.

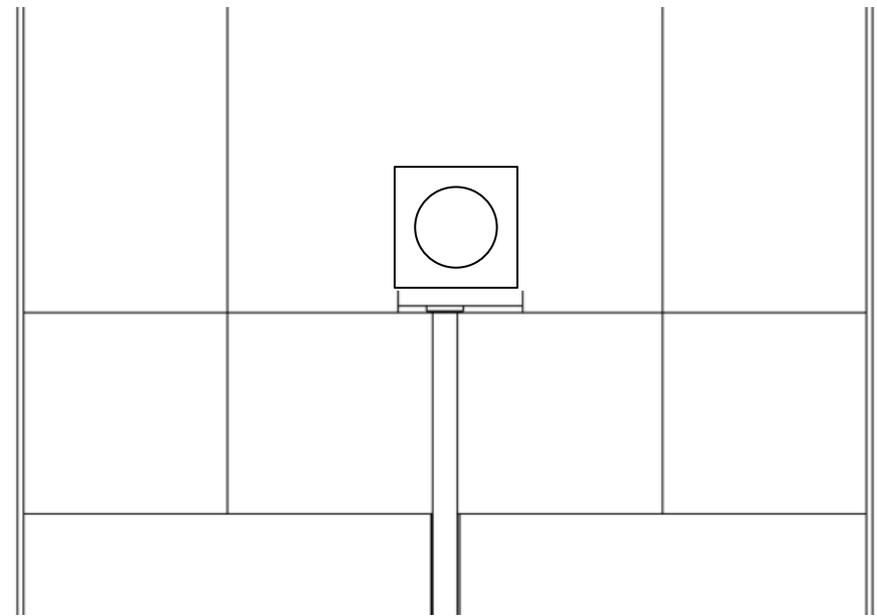


Solution to be discarded because of the huge flow rate of compressed needed (~**10000 m<sup>3</sup>/h**) and the energy needed (to compress + dry).

## Air-cooling

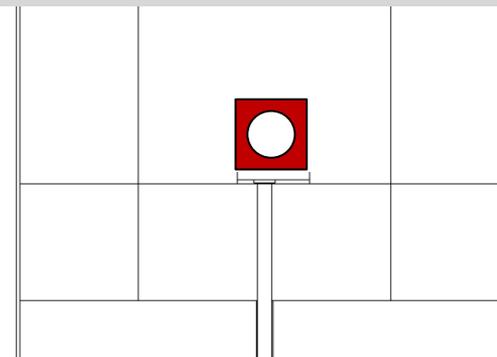


## Liquid-cooling



## ASSUMPTIONS

- Pipe dimensions: 4 mm i.d. (round)
- Refrigerant velocity:  $1.5 \text{ m s}^{-1}$
- Refrigerant temperature:  $-50^\circ\text{C}$
- Cooling load per module: 10 W



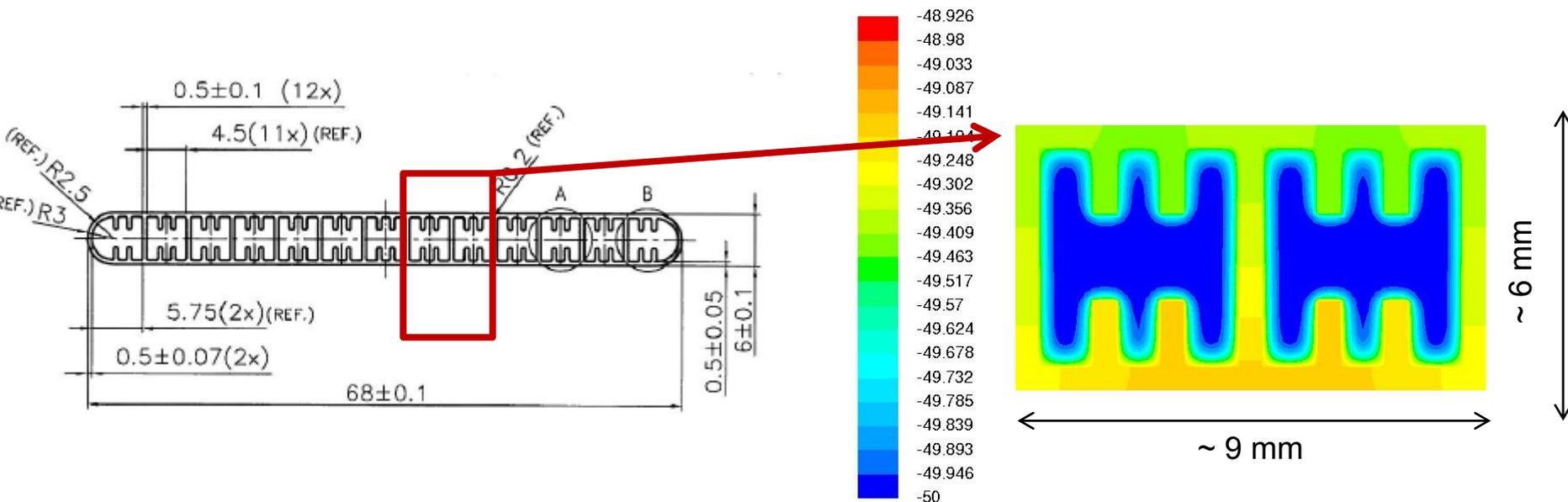
Refrigerant	$\Delta T_{\text{out-in}}$ [K]	HTC [ $\text{W m}^{-2} \text{K}^{-1}$ ]	$\Delta T_{\text{wall-ref}}$ [K]	$\Delta p$ [bar]	Flow Rate [ $\text{kg s}^{-1}$ ]
Dynalene*	0.36	120	12	0.20	0.015
Dowterm J**	0.35	138	11	0.06	0.017
$\text{C}_6\text{F}_{14}$	0.3	1200	1.3	0.10	0.035
NOVEC649	0.28	1100	1.4	0.11	0.034
$\text{CO}_2$ liquid***	0.24	6000	0.3	0.004	0.022
$\text{NH}_3$ liquid****	0.17	11000	0.14	0.005	0.013

\* Aliphatic hydrocarbon blend

\*\* Mixture of isomers of an alkylated aromatic

\*\*\* Saturation pressure @  $30^\circ\text{C}$ : 72 bar, freezes at  $-56^\circ\text{C}$  \*\*\*\* Saturation pressure @  $30^\circ\text{C}$ : 11.6 bar; copper must be avoided

- The “default” CERN solution for single-phase detectors cooling ( $\text{C}_6\text{F}_{14}$ ), as well as its “green” substitute (NOVEC649), would fit without problem;
- Fluids such as Dynalene or Dowterm J display low HTC and may need an higher heat transfer surface.
- $\text{CO}_2$  and  $\text{NH}_3$  display thermodynamic properties far better than what needed;
- Almost any two-phase cooling option would work with this configuration;



Contours of Static Temperature (c)

Fluid	Velocity [m s <sup>-1</sup> ]	$\Delta T_{out-in}$ [K]	$\Delta T_{wall-ref}$ [K]	$\Delta p$ [bar]	Flow Rate [kg s <sup>-1</sup> ]
Dynalene	1	0.17	<b>1.4</b>	0.31	0.0320
Dowtherm-J	1	0.17	<b>1.3</b>	0.10	0.0357

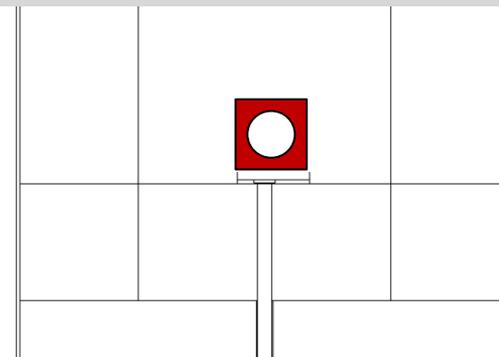
➤ Low HTC issue can be easily solved by increasing the heat transfer surface.

## B. CONCLUSIONS

- Requirements in terms of cooling load and power density ( $O(10W)$  over 0.5 m length) and temperature uniformity (10 K per module) are not very demanding;
- Air-cooling with vortex tubes could in principle cope with these requirements, but this solution is to be discarded because of the huge amount of compressed air needed ( $O(10000 \text{ m}^3/\text{h})$  with  $-70^\circ\text{C}$  dew point);
- Liquid-cooling with  $\text{C}_6\text{F}_{14}$  or NOVEC649 would fit the requirements in terms of heat transfer coefficient and silicon die temperature uniformity;
- Depending on the fluid used, a round 4 mm pipe or a multiport pipe (augmented heat transfer surface) may be needed;
- From the point of view of the heat transfer process inside the module, there is absolutely no need to use “high-performance” solutions such as evaporative cooling.

# THANKS FOR YOUR ATTENTION

# BACK-UP SLIDES

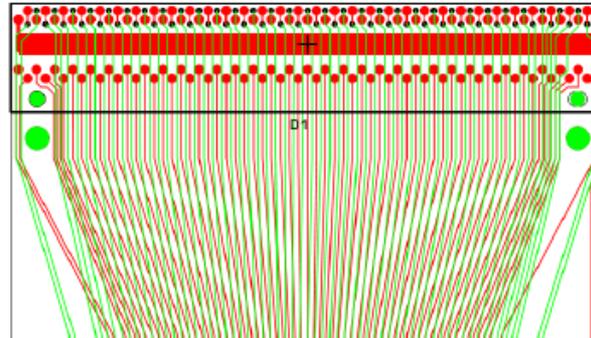
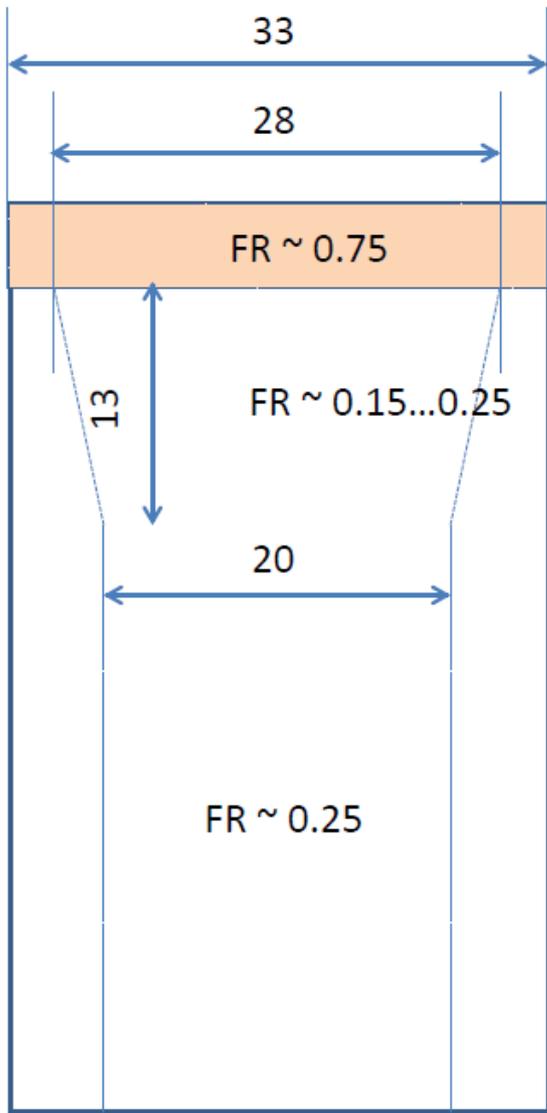


Fluid	$\Delta T_{\text{out-in}}$ [K]	HTC [ $\text{W m}^{-2} \text{K}^{-1}$ ]	$\Delta T_{\text{wall-ref}}$ [K]	$\Delta p$ [bar]	Flow Rate [ $\text{kg s}^{-1}$ ]
Water/70% methanol *	0.17	354	4.3	<b>0.54</b>	0.018
Water/29.9% calcium chloride **	0.15	463	3.3	0.36	0.025
Syltherm XLT	0.40	111	<b>14</b>	0.09	0.017
Thermogen VP1869	0.25	158	<b>10</b>	<b>0.80</b>	0.019
Dynalene	0.36	120	<b>12</b>	0.20	0.015
Dowterm J	0.35	138	<b>11</b>	0.06	0.017

\* Minimum temperature  $-57^{\circ}\text{C}$

\*\* Minimum temperature  $-55^{\circ}\text{C}$

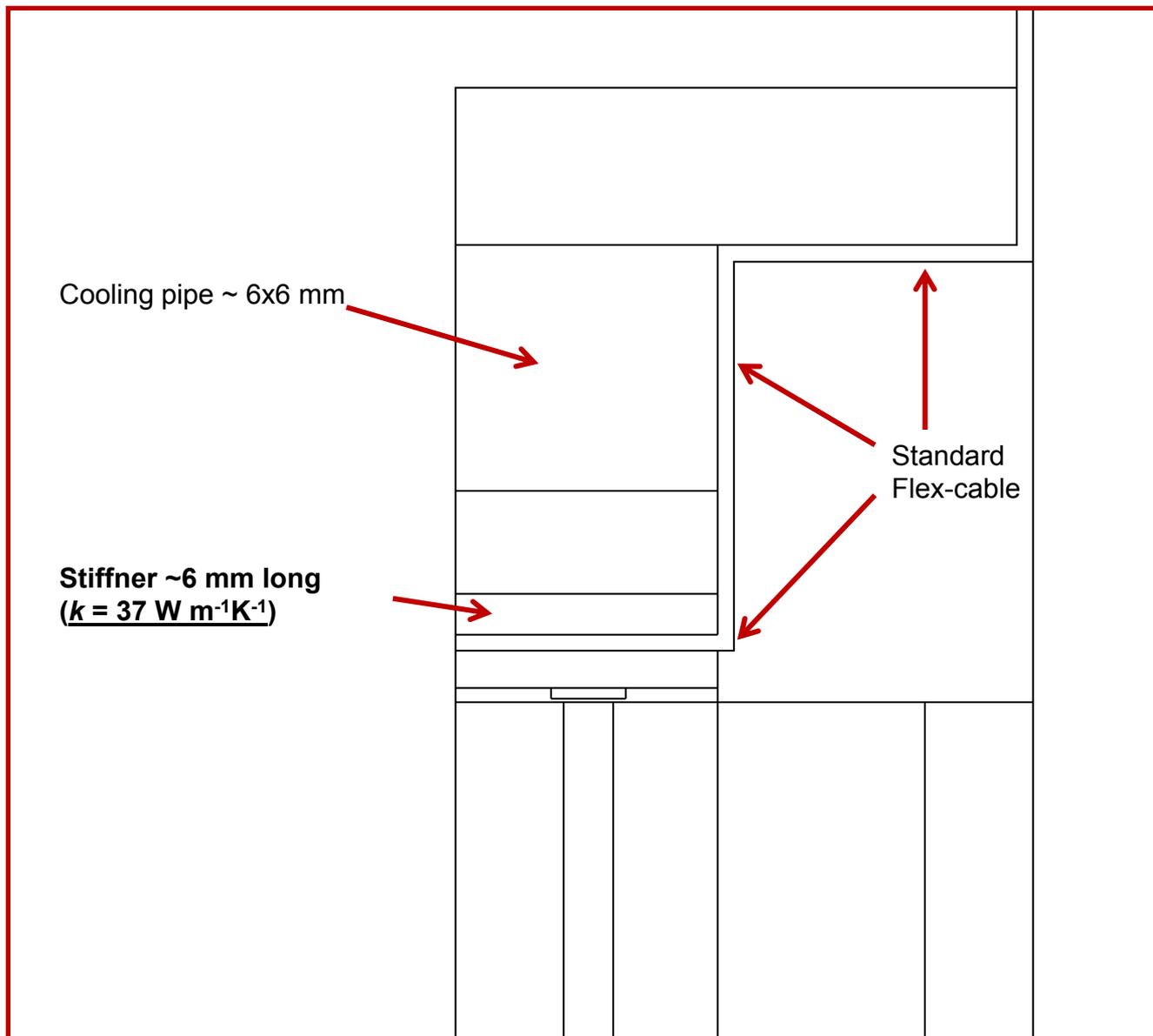
- Water mixtures with methanol or calcium chloride would work, but the freezing point  $\sim -55^{\circ}\text{C}$  could be a problem.

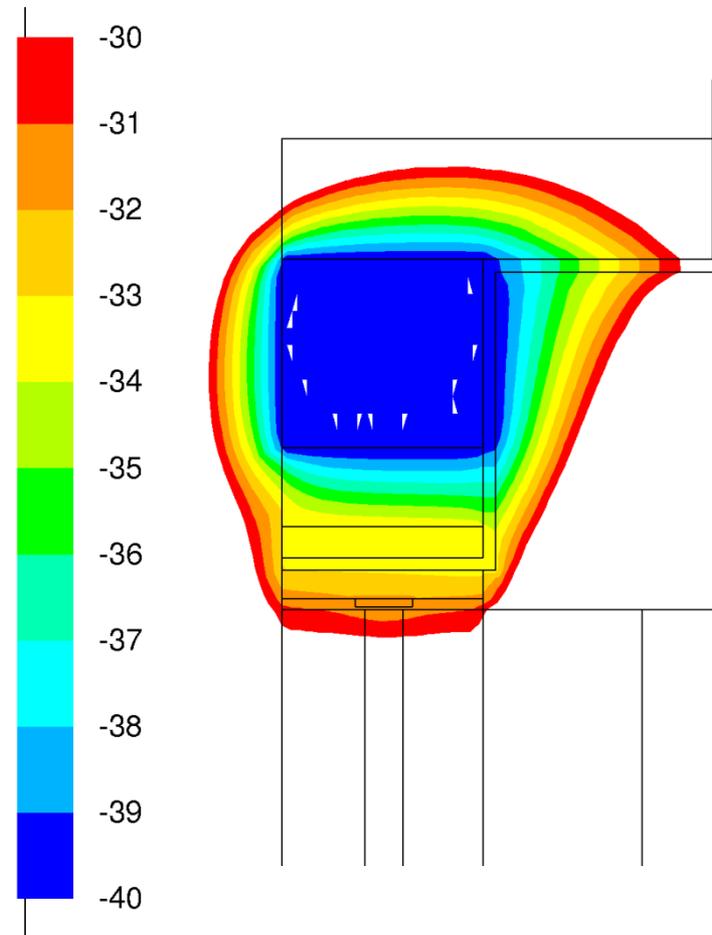
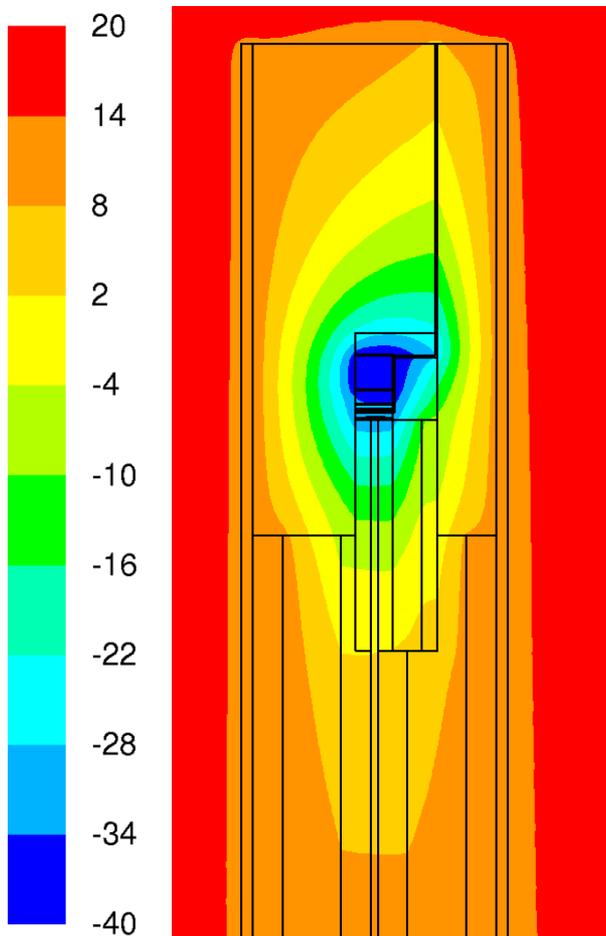


FR=fill ratio = copper/empty  
 130 conductors, 75 um wide, 20 um thick  
 IMO, a reasonable approximation would be a bulk copper band, 28x5.56 mm<sup>2</sup>



20 um copper, impressed into coverlay





**Silicon die: -32°**

- Copper must be added to the flex-cable in order to reduce the refrigerant-to-silicon temperature difference.